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1 **Thermohydraulic analysis of a microchannel with varying superhydrophobic roughness**

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11  
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13  
14 **Abstract**

15 Nature inspired superhydrophobic surfaces are applied to microchannels to minimize the pumping power needed for  
16 driving the fluid flow. Special attention is given to the superhydrophobic surfaces with alternative microstructures and  
17 four different micro-structured configurations including square and triangular micro-posts and micro-holes are  
18 examined in aligned and staggered patterns. A numerical study is conducted to identify the impact of cavity fractions  
19 of 0.1 to 0.9 and Reynolds numbers of 10 and 100 on the performance indicators. These include drag reduction, heat  
20 transfer rate and mixed hydraulic and thermal behavior of the microchannel evaluated by the thermal performance  
21 index. The results reveal that the Poiseuille and Nusselt numbers decrease by the increase of cavity fraction. It is also  
22 observed that the triangular patterns feature the best thermal performance. The optimal combination of heat transfer  
23 and pressure drop, reflected by the goodness factor, can be achieved in staggered square holes and posts patterns at  
24 low and high Reynolds numbers, respectively. Considering the total thermal performance of the microchannel,  
25 changing the microstructures from aligned to staggered pattern can have a significant influence upon the square micro-  
26 posts and micro-holes but only a modest impact on the triangular posts. Nonetheless, the optimal surface configuration  
27 should be picked up in accordance with the specific application in hand and by prioritizing improvements in thermal  
28 or hydraulic performance of the microchannel.

29  
30 **Keywords:** Superhydrophobic surface (SHS); Poiseuille and Nusselt number; Slip length; Microchannel; square and  
31 triangle microstructures; goodness factor.

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32  
33 **Nomenclature**

$A$	cross-sectional area of flow (m <sup>2</sup> )	$P_w$	liquid perimeter
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$A_c$	shear-free area (m <sup>2</sup> )	$\bar{q}''$	average heat flux (W/m <sup>2</sup> )
$A_t$	total wall area (m <sup>2</sup> )	$Re$	Reynolds number
$C_p$	specific heat at constant pressure (j/kg/K)	SHS	superhydrophobic surface
$D_h$	hydraulic diameter (m)	$T$	fluid temperature (K)
$f$	friction factor	$\bar{T}_m$	fluid mean temperature (K)
$F_c$	cavity fraction	$T_s$	temperature of no-slip wall (K)
$F_s$	solid fraction	$u_m$	mean velocity of fluid flow (m/s)
$H$	microchannel height	$u_s$	Slip velocity (m/s)
$i$	$x$ -direction component	$w$	solid-cavity width (m)
$j$	$y$ -direction component	$W_r$	relative pattern width
$k$	fluid thermal conductivity (W/m/K)	$\eta$	thermal performance index
$L$	solid-cavity length (m)	$\lambda$	Slip length (m)
<i>MEMS</i>	microelectromechanical systems	$\mu$	fluid dynamic viscosity (kg/m/s)
$\dot{m}$	mass flow rate (kg/s)	$\rho$	fluid density (kg/m <sup>3</sup> )
$Nu$	Nusselt number	$\tau_w$	wall shear stress (N/m <sup>2</sup> )
$Po$	Poiseuille number	$\varphi$	goodness factor
$Pr$	Prandtl number	$\varphi_c$	smooth channel goodness factor

34

## 35 1. Introduction

36 Microdevices continue to receive a significant attention worldwide. These devices have found various  
37 applications in a number of emerging technologies including microfluidic systems, microelectromechanical  
38 technology (MEMS) and microchemical reactors. Further, microchannels are applicable in cooling of electrical  
39 devices [1] and have a high heat transfer coefficient due to their large surface to volume ratios. Microchannel can be  
40 assumed as a heat exchanger, which can be found in different types like circular tube [2,3] integrated with alternative  
41 inserts [4–6], double-layer microchannel heat sink [7], solar-based heater [8,9]. Heat transfer coefficient and shear  
42 stress increase as the hydraulic diameter of the microchannel decreases [10]. Consequently, pressure losses through  
43 microchannels are quite significant and demand a large pumping power, which is clearly a major drawback.

44 To address this issue, employing nature inspired superhydrophobic surfaces (SHSs) found on a lotus, rice leaf,  
45 butterfly wings, lizard skin, collembolan, shark skin, fish scale, red rose petal, poplar leaf [11], appeared to have a  
46 significant potential. On SHSs, the contact angle of droplet transgresses 150°, which could be made by capillary  
47 coatings, spray coating, chemical etching, solution immersion, laser electrodeposition, sol-gel, atmospheric pressure  
48 plasma, photolithography and colloidal assemblies [12,13]. It is worth mentioning that SHSs have a large number of  
49 applications including producing self-cleaning, anti-icing, anti-corrosion [14], anti-fouling, anti-reflective [15] and  
50 anti-fogging surfaces as well as liquid transport and separation [16], water collection and biomedical applications [17].  
51 These have turned SHSs into an exciting and largely unexplored research topic.

52

### 53 1.1. Literature review

54 Drag and friction can often cause major engineering challenges. Shear stress is responsible for about 50% of drag  
55 on ships [18] and leads to consumption of a large amount of energy in industrial processes. [Water is considerably](#)  
56 [utilized to transfer waste thermal energy to the environment \[19\]](#). On SHSs, air is trapped between  
57 nano/microstructures and due to surface tension and their small size, water infiltration into micro holes is not possible.  
58 This constitutes a shear-free air-water interface and therefore reduces the flow friction. This state is known as Cassie-  
59 Baxter [20], where liquid droplets remain at the top of roughness. Alternatively, liquid droplet penetrates the  
60 microstructure and lead to Wenzel's state [21]. [Ou et al. \[22\] carried out an experiment and reported the pressure drop](#)  
61 [and slip length for SHS with the cavity fractions in access of 0.95](#). As solid-water interface (wetted contact area)  
62 decreases, a drop in the pressure loss and a convenient fluid flow through microchannels becomes achievable [23].

63 A large number of investigations have been already carried out on various SHS structures, flow and boundary  
64 conditions. Maynes et al. [24] analyzed longitudinal rib and cavity walls in microchannels with laminar flow  
65 analytically. Teo and Khoo [25] as well as Cowley et al. [26] examined this phenomenon with transverse grooves and  
66 square pillars, respectively. Haghighi et al. [27] explored the effect of superhydrophobicity on the axial hydraulic  
67 turbine by entropy generation method. Krishnan et al. [28] observed the improvement of 97% in heat flux and 88% in  
68 heat transfer coefficient by silane coating of picosecond laser-treated SHS. Another interesting study indicated that  
69 air conditioner efficiency could be enhanced by using SHSs in heat exchanger [29].

70 Choi et al. [30] revealed that trapped air between grooves could be depleted by high-pressure gradient although  
71 this issue can be addressed by cutting down the length and width of the cavities. In Norouzi et al. [31] study, the  
72 maximum drag reduction was attainable when the fluorocarbon compound as a water repellent was used on the pre-  
73 treated surface. This is because of the creation of microbubbles between substrate and water flow that leads to water  
74 slippery over the surface and thus more reduction in drag. Tuo et al. [32] fabricated anisotropic SHS on stainless steel  
75 comprising inclined grooves by laser etching and fluoride treating for drag test. Comparing inclined and reversed  
76 direction of ribs, while drag-drop ratio in the first situation is about 18%, it is almost 48% in the latter under 4.48m/s  
77 flow velocity. Tuo et al. [33] used aluminum foil and one-step hydrothermal mechanism to prepare their SHS by  
78  $\text{Al}[\text{CF}_3(\text{CF}_2)_{12}\text{COO}]_3$  with small sliding angle and huge contact angle resulting in almost 20-30% drag reduction at 2-  
79 5m/s fluid velocity.

80 Considering turbulent flows, Rastegari and Akhavan [34] conducted a numerical work on high Reynolds number  
81 flows in which they investigated drag reduction of micro-posts and microgrooves aligned with flow direction. They  
82 observed that drag reduction and the sustainability bounds of SHS deteriorate as the Reynolds number increases.  
83 Rajappan et al. [35], found that for a turbulent flow, small surface roughness, a large autocorrelation length as well as  
84 hierarchical roughness are necessary to achieve excellent drag reduction along with having a Cassie-Baxter state [36].  
85 Also, these authors pointed out that to overcome the depletion of air trapped among microstructures, as a necessity for  
86 superhydrophobicity maintenance, further investigations should be carried out in turbulent flows and their feasibility.  
87 However, some strategies have been under investigation to tackle this issue. Gose et al. [37] showed that for reaching  
88 the desired drag reductions in turbulent flows, surface roughness and the contact angle hysteresis (CAH) should be  
89 minimized. In their study, 50% reduction in drag was achieved in high-velocity turbulent flows like those related to

90 naval applications. Moreover, a higher heat transfer can be reach by using alternative working fluid like nanofluids  
91 [38].

92

### 93 1.2. Objectives

94 The review of literature revealed that there is an extensive room to produce commercial and sustainable SHSs for  
95 diverse applications. Some durable and cost-effective SHSs prepared with advanced methods have been tested for  
96 certain purposes targeting mechanical or chemical fabrication process, anti-corrosive, anti-icing, anti-fungal, anti-  
97 fogging or self-cleaning surfaces, which are worth examining in other applications. This approach has addressed a  
98 wide range of technical issues in many fields ranging from daily life to industry and medicine. Importantly, some  
99 kinds of SHSs seem to be durable and applicable in one area but fail in other functions. This sensitivity calls for careful  
100 experimental and numerical analyses before mass production of such surfaces. There have been extensive  
101 investigations on SHSs comprising micro-posts [39–41], micro-holes [42], transverse [25,43] or longitudinal  
102 (streamwise) ribs and cavities [24,44,45] produced physically or chemically. Each of them focuses on a particular  
103 aspect of fluid flow over SHSs such as friction factor, slip and temperature jump length. However, investigations on  
104 other geometries have, so far, received much less attention. From which, triangular patterns have drawn few thermal  
105 and hydraulic considerations.

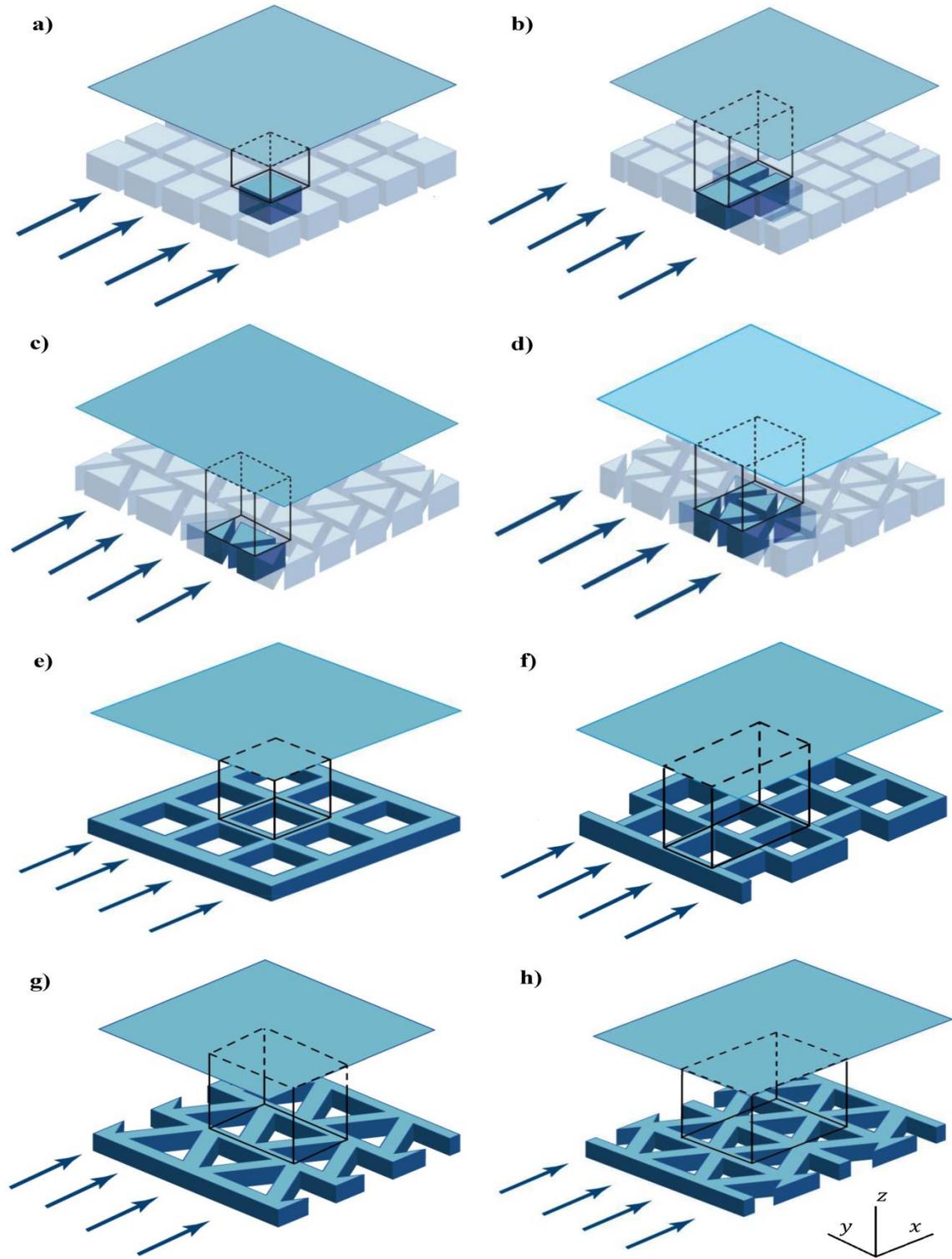
106 Augmentation of heat transfer has been the focus of a number of studies including the recent work of Ryu et al.  
107 [46] on improvement of heat transfer by microstructures. The promising heat removal effect of SHS with aligned  
108 micro-posts in microchannels comparing with that of conventional microchannels was shown by Cheng et al. [47].  
109 They also indicated that the Nusselt number rises by accelerating and decelerating the flow through the microchannel.  
110 Taking advantage of different types of roughness could make the flow acceleration and deceleration achievable.  
111 Further, staggering the roughness can be seen as a viable route to reaching higher Nusselt numbers, as the flow  
112 experiences more acceleration and deceleration, while there is an almost little frictional resistance. In the current study,  
113 it is attempted to carry out numerical work on the role of SHSs in drag reduction and heat transfer within  
114 microchannels. To show the superiority of the proposed SHSs, the results on Poiseuille and Nusselt number as well  
115 as the total thermal index are compared to those of conventional surfaces. The survey of literature revealed that, so  
116 far, little attention has been paid to alternative roughness and especially to the staggered triangular microstructure.  
117 Therefore, the proposed microstructures are SHSs with square and triangular micropillars and micro-holes. This study  
118 aims to broaden the current horizons in adoption of SHSs to overcome commercial and industrial barriers. Finally,  
119 even though SHSs are examined for drag reduction and heat transfer, their other advantages should not be overlooked.  
120 These include being self-cleaner, anti-corrosive, anti-fouling and so on, which foster further research to exploit these  
121 versatile SHSs.

122

## 123 2. Methodology

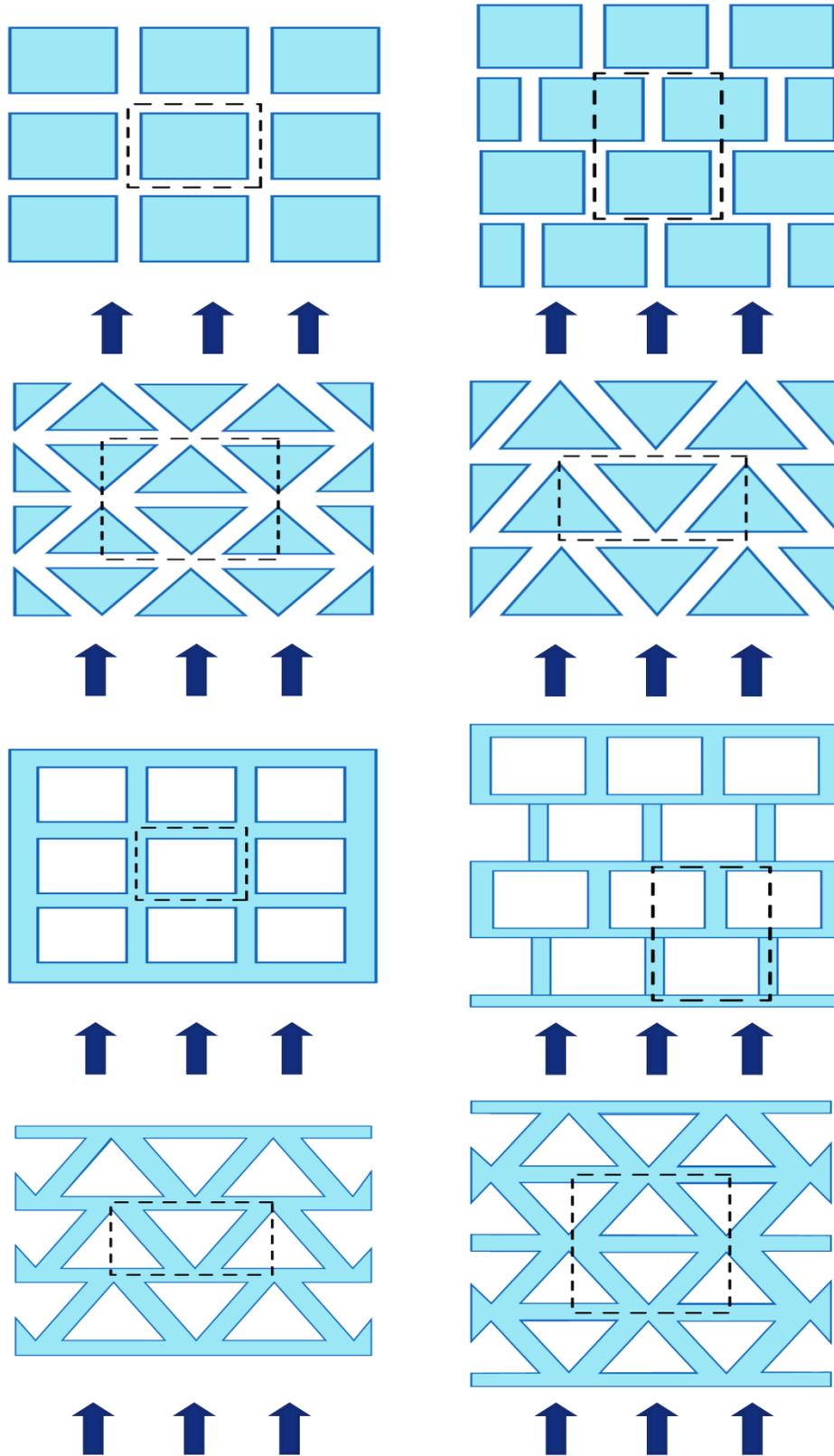
124 SHSs with four different microstructures, namely square and triangular micro-holes and micro-posts on a lattice,  
125 are employed to investigate drag reduction and heat transfer in a microchannel. The proposed geometries and mesh  
126 were generated in ANSYS Gambit 2.4.6. The schematics of the aligned and staggered roughness are depicted in Fig.

127 1. Due to symmetry, only half of the height of microchannel ( $H/2$ ) was simulated. Fig. 2 illustrates the computational  
128 domains in dotted and solid lines with width of  $W$ , length of  $L$  (equal to  $W$  for square patterns) and the relative pattern  
129 width can be defined as  $W_r = W/D_h$ . The hydraulic diameter ( $D_h = 4A/P_w$ ) can be equated to  $2H$  considering an  
130 infinite width of microchannel, where  $A$  and  $P_w$  denote flow cross area and fluid perimeter, respectively.  
131



132  
 133  
 134  
 135  
 136

**Fig. 1.** SHSs microstructures a) aligned square micro-posts, b) staggered square micro-posts, c) aligned triangular micro-posts, d) staggered triangular micro-posts, e) aligned square micro-holes, f) staggered square micro-holes, g) aligned triangular micro-holes and h) staggered triangular micro-holes. Fluid flow is shown with arrows and symmetric plane by the upper surfaces.



137  
 138  
 139

**Fig. 2.** Top view of SHSs for different patterns with flow direction and computational domain. Each domain has a width of  $W$ .

140 Cavity fraction and Reynolds number are defined as  $F_c = A_c/A_t$  and  $Re = \rho \bar{u}_m D_h / \mu$ , where  $A_c$ ,  $A_t$ ,  $\bar{u}_m$ ,  $\rho$  and  
 141  $\mu$  are the cavity area, surface area of the microchannel wall, mean fluid velocity, fluid density and dynamic viscosity,  
 142 respectively. To identify the effect of SHSs with various microstructures on the pressure drop and heat transfer through  
 143 the microchannel, Poiseuille number and Nusselt number were investigated. These are constant in conventional  
 144 channels with fully developed laminar and incompressible flows. The production of friction factor and Reynolds  
 145 number lead to Poiseuille number ( $Po = fRe$ ) and will be evaluated in a few cases to represent the strength of different  
 146 geometries on drag reduction. Friction is deemed to be a serious issue hindering fluid flow in micro/nanodevices, and  
 147 therefore should be addressed effectively to reduce pumping energy. The friction factor is defined as

$$f = 8 \bar{\tau}_w / \rho \bar{u}_m^2, \quad (1)$$

148 where  $\bar{\tau}_w$  and  $\rho$  are the average wall shear stress and fluid density. Slip length, defined as the normal distance from  
 149 wall to where streamwise velocity diminish, can be calculated in terms of gradient of fluid velocity  $l$  and slip velocity  
 150 on the channel wall by [48]:  
 151

$$\lambda = \frac{u_s}{\left(\frac{\partial u}{\partial z}\right)}. \quad (2)$$

152 To evaluate the thermal performance of SHSs, the proposed formula for Nusselt number by Enright1 et al. [49] can be  
 153 used. This reads:  
 154

$$Nu = \frac{\bar{q}'' D_h}{k(\bar{T}_s - \bar{T}_m)}, \quad (3)$$

155 in which  $k$  is the fluid thermal conductivity,  $\bar{q}''$  is the average heat flux imposed on the microchannel wall,  $\bar{T}_s$  is the  
 156 mean temperature of no-slip (solid) part of SHS and  $\bar{T}_m$  is the average temperature of the fluid through the  
 157 microchannel. The local friction factor and Nusselt number can be represented at each point as:  
 158

$$f_x = 8 \bar{\tau}_{w,x} / \rho \bar{u}_m^2, \quad (4)$$

159 and

$$Nu_x = \frac{\bar{q}_x'' D_h}{k(\bar{T}_{s,x} - \bar{T}_{m,x})}. \quad (5)$$

160 Maynes et al. [24] showed that the effect of meniscus angles is just less than 4% for fully developed laminar flow in  
 161 microchannel. Therefore, the solid-liquid interface assumed to be due to the trivial amount of difference between  
 162 viscous and surface tension forces [47]. On the basis of the existing theories, the supportable pressure by air-water  
 163 interface could be calculated by Young's law [50]. As the cavities and distances between posts are in the order of  
 164 micro-meter and microchannels with SHS experience less frictional resistance, the Cassie state [51] is considered here.  
 165 This expresses that with the help of surface tension the liquid does not penetrate into the cavities [40]. Further, since  
 166 liquid penetration into the cavities depends upon various factors such as manufacturing methods and quality, type of  
 167 materials, liquid surface tension and flow pressure, new methods have been proposed to increase the  
 168 superhydrophobicity of the surfaces and liquid-air durability [52–54]. For example, Carlborg et al. [55] showed that  
 169 air pockets on a modified surface could support liquid pressures that are three times higher than the theoretical  
 170

171 predictions. Further, as mentioned earlier, a cavity fraction of more than 0.95 was studied experimentally [22], the  
 172 maximum cavity fraction is considered to be 0.9 in the current study. Although the maximum amount of pressure drop  
 173 is less than 5 kPa and the supportable pressure by air-water interface could be calculated by Young's law [50], Samaha  
 174 et al. [53] were able to reach proper drag reduction under the hydrostatic pressure of 600 kPa.

175  
 176 2.1. Numerical method

177 To evaluate the effect of different geometries and patterns, five cavity fractions of 0.1, 0.3, 0.5, 0.7 and 0.9 under  
 178 incompressible and laminar flow with Reynolds numbers of 10 and 100 are considered. Hydraulic diameter is 1 mm,  
 179 relative pattern width is 1, inlet flow temperature is 300 K and constant wall heat flux justified to be 70000 W/m<sup>2</sup>.  
 180 The Nusselt number is independent of the amount of heat flux and it is just a function of cavity fraction [49] and is  
 181 selected to be small enough to prevent water boiling at the outlet of the microchannel. The width and length of the  
 182 computational domain for square posts will be 1 × 1 mm and for triangular posts is 1 × 0.866 mm with the same  
 183 height of 0.25 mm. Constant surface heat flux is applied on the no-slip (solid) part of SHS and is small enough for  
 184 fluid flow to prevent reaching saturation temperature. The cavity-liquid interface assumed to be adiabatic and shear  
 185 free (slip condition) surface. The finite-volume approach by ANSYS Fluent 6.3.26 was utilized for numerical solution  
 186 of fluid flow and heat transfer in microchannel. Considering discretization of momentum and energy equations, the  
 187 second order upwind method was employed along with SIMPLEC algorithm for the pressure-velocity coupling.

188  
 189 2.2. Governing equations and boundary conditions

190 Water is considered as the working liquid. Considering constant properties ( $\rho =$   
 191 998.2 kg/m<sup>3</sup>,  $\mu = 0.001003$  kg/m<sup>m</sup>/s,  $k = 0.6$  W/m/K and  $C_p = 4180$  J/kg/K) and being an incompressible, the  
 192 following equations are solved.

193 Continuity of mass:

$$\frac{\partial(u_i)}{\partial x_i} = 0. \tag{6}$$

194  
 195 Transport of fluid momentum in three dimensions:

$$\rho \frac{\partial(u_i u_j)}{\partial x_i} = \mu \frac{\partial}{\partial x_i} \left( \frac{\partial u_j}{\partial x_i} \right) - \frac{\partial p}{\partial x_j}, \tag{7}$$

196  
 197 and transport of fluid energy:

$$\frac{\partial(u_i T)}{\partial x_i} = \frac{k}{\rho C_p} \frac{\partial}{\partial x_i} \left( \frac{\partial T}{\partial x_i} \right). \tag{8}$$

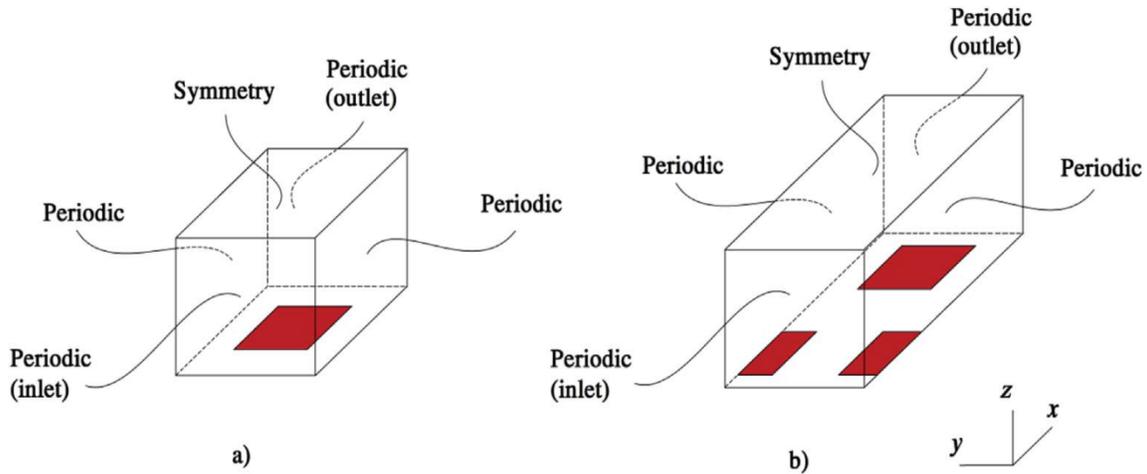
198  
 199 In Eqs. (5-7), fluid viscosity, thermal conductivity, specific heat at constant pressure, fluid temperature, component  
 200 of flow velocity in direction of  $x$  and pressure are denoted by  $\mu$ ,  $k$ ,  $C_p$ ,  $T$ ,  $u_i$  and  $p$ , respectively.

201 As there are translationally periodic geometries, the inlet / outlet and sides of the computational domain are  
 202 defined as periodic boundaries for all cases. To validate this boundary condition, the complete lengths of the

203 microchannels were simulated for some cases and the results showed a good agreement with periodic inlet/outlet  
 204 boundary condition for both Nu and fRe. Symmetry boundary was applied to the above surface at the height of  $H/2$   
 205 due to facing the symmetry conditions in the current study. The solid portion with no-slip condition and air-packed  
 206 region with free-shear stress are depicted in Fig. 3 for the aligned and staggered square micro-posts. The red portions  
 207 indicate the solid part of liquid-solid interface with constant heat flux. The remaining areas are air-liquid interface  
 208 assumed to be adiabatic as a result of small thermal conductivity of air in comparison with water. To ensure  
 209 acceptability of the results and convergence, the simulations were regarded as converged with the residuals being less  
 210 than  $10^{-8}$ . Fluid flow with specific Reynolds number within the microchannel was achievable by applying pressure  
 211 gradient and mass flow rate on the inlet and outlet periodic boundary conditions. The desirable mass flow rate can be  
 212 calculated by the mean velocity of fluid flow ( $\overline{u}_m = Re\mu/\rho D_h$ ) through the cross-section area of microchannel ( $A$ )  
 213 at  $Re = 10$  and  $100$  by:

$$\dot{m} = \rho A \overline{u}_m \quad (9)$$

215



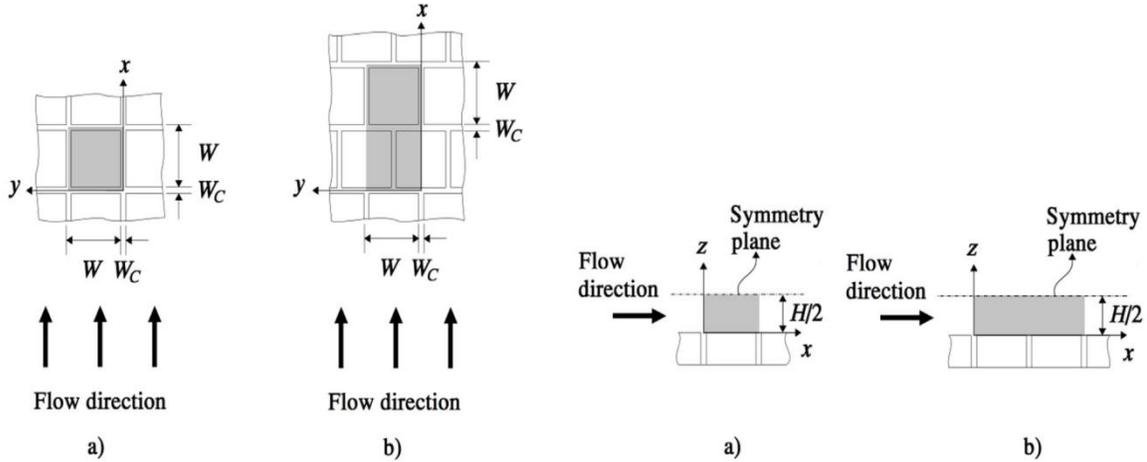
216

217 **Fig. 3.** Computational domains for a) aligned square micro-post b) staggered square micro-post.

218

219 The top and right views of the computational domain are also represented in Fig. 4 for aligned and staggered  
 220 square micro-posts. The computational domains are demonstrated in dark areas.

221

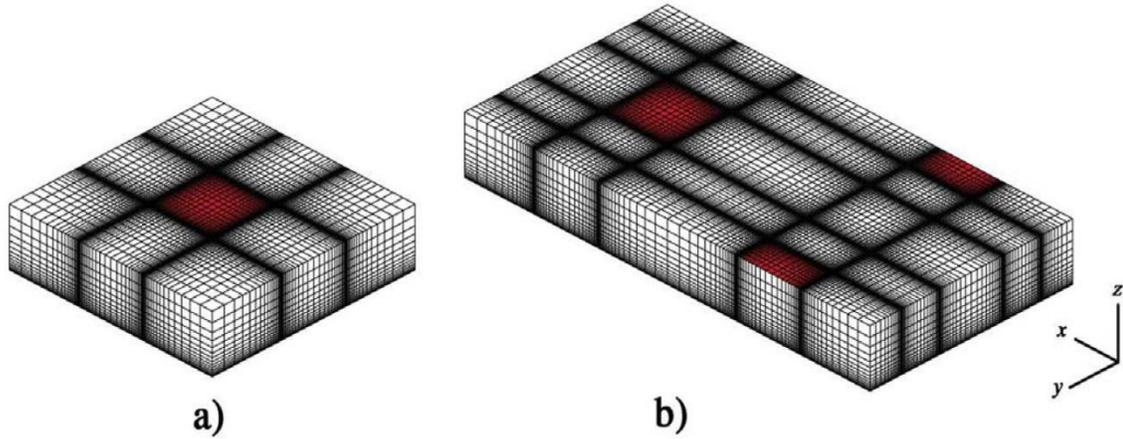


222  
 223 **Fig. 4.** Top and right views for a) aligned b) staggered square micro-post. Grey areas illustrate the computational  
 224 domain.

225  
 226 2.3. Grid independency and validation

227 A structured grid was generated for microchannels with square posts and holes and a hexa mesh for triangular  
 228 part of the microchannels with triangular micro-posts and micro-holes. The concentrated grids were adopted near the  
 229 edges due to the high variation in fluid flow. The grid independency study was carried out using refined and coarse  
 230 meshes under Reynolds number of 100 at cavity fraction of 0.1 and 0.9, where the strongest gradients occur, to  
 231 compare the values of Poiseuille and Nusselt number for all geometries.

232 To illustrate structure of the generated grid, Fig. 5 presents the coarse grid for aligned and staggered square  
 233 patterns of micro-posts at cavity fraction of 0.9. The surface of solid portions of SHS are at the opposite side of the  
 234 red portions of symmetry plane at the lowest part of the computational domain. Table 1 shows the results of grid  
 235 independency study for the aligned and staggered micro-posts and at Reynolds number of 100 and cavity fractions of  
 236 0.1 and 0.9, respectively. This suggested that the coarse grid offers acceptable results with just less than 3% differences  
 237 with the refined mesh for both aligned and staggered configurations. The adopted grid size in the  $x$ ,  $y$  and  $z$  directions  
 238 for the square patterns are  $60 \times 60 \times 13$  and  $118 \times 92 \times 15$ , and for triangular patterns are  $64 \times 46 \times 13$  and  $64 \times 92 \times$   
 239  $13$  in the aligned and staggered configurations, respectively.



241  
242 **Fig. 5.** Coarse grid utilized for grid study at  $F_c = 0.1$ . a) aligned b) staggered square micro-post.

243  
244 **Table 1**  
245 The Poiseuille and Nusselt numbers of aligned and staggered patterns of micro-post for the refined and coarse grids  
246 at Reynolds number of 100 and  $F_c = 0.1$ .

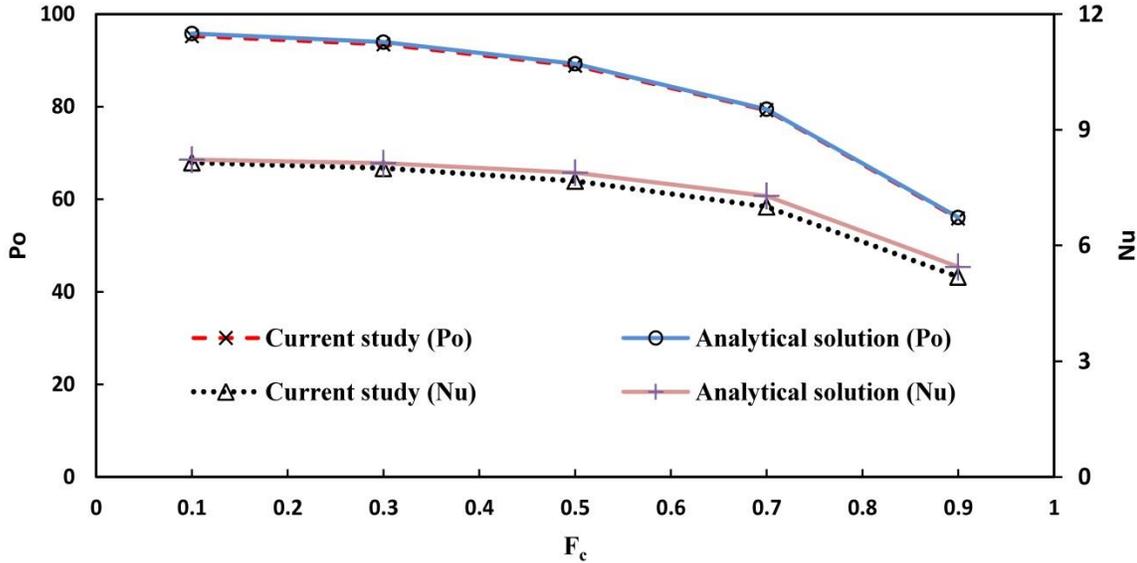
	Aligned				Staggered			
	Refine		Coarse		Refine		Coarse	
	Po	Nu	Po	Nu	Po	Nu	Po	Nu
Square post	93.9	8.02	93.3	7.99	93.9	8.08	93.4	8.05
Square hole	91.5	7.8	90.9	7.86	91.1	8.03	91	8.03
Triangular posts	91.1	8.11	93.9	8.11	94.3	8.1	93.9	8.1
Triangular holes	92	8.02	91.98	8.03	92.3	8.02	92	8.03

247  
248  
249 **Table 2**  
250 The Poiseuille and Nusselt numbers of aligned and staggered patterns of micro-post for the refined and coarse grids  
251 at Reynolds number of 100 and  $F_c = 0.9$ .

	Aligned				Staggered			
	Refine		Coarse		Refine		Coarse	
	Po	Nu	Po	Nu	Po	Nu	Po	Nu
Square post	14	1.55	13.8	1.54	18.6	2.64	18.3	2.6
Square hole	29	2.67	28.9	2.71	30.2	47	29.8	3.51
Triangular posts	22.7	2.87	22.5	2.88	22.6	2.83	22.4	2.9
Triangular holes	38.7	5.28	37.3	5.27	38.4	4.91	37	5.03

252  
253 As mentioned earlier, Enright et al. [49] developed an analytical solution for the Nusselt and Poiseuille numbers  
254 in microchannels (among two parallel plates extended to infinity) with aligned square micro-post. Their solution is a  
255 function of the thermal and hydrodynamic slip length on the channel wall. This was obtained under some conditions  
256 that are valid for solid fraction ( $F_s = A_{solid}/A_{wall}$ ) less than 0.9, where the diffusive heat transfer is dominant at  
257 creeping flow near SHS ( $Re_w = \rho W \tilde{u}_w / \mu \rightarrow 0$ ). Therefore, the numerical solutions were validated for  $Re = 10$  and

258 relative pattern width of 0.01, where the low amount of  $Re_w$  was accessible through the performed numerical study.  
 259 Fig. 6 demonstrates a good agreement between the outcomes of the current numerical simulations and those of the  
 260 analytic work of Enright et al. [49]. This agreement confirms capability of the current numerical simulations in  
 261 analyzing laminar fluid flows with different patterns of microstructures.  
 262



263  
 264  
 265 **Fig. 6.** Comparison between the Nusselt and Poiseuille numbers obtained from the numerical and theoretical  
 266 approaches [49].  
 267

268 **3. Results and discussion**

269 In this section, diverse parameters are calculated numerically for four various patterns on SHS to analyze the  
 270 effects of different geometries on drag reduction and heat transfer within the microchannel. Then, the total  
 271 performance of SHS on simultaneous drag reduction and heat transfer enhancement will be discussed in the context  
 272 of goodness factor.  
 273

274 **3.1. Drag reduction**

275 Fig. 7 represents Poiseuille number versus different cavity fractions at Reynolds number of 10 and 100 for aligned  
 276 and staggered patterns of microstructures. As can be seen, the Poiseuille number approaches 96 (an amount of Po in  
 277 conventional channels) as the cavity fraction becomes smaller. Shear free interface increases as the cavity fraction  
 278 rises from 0.1 to 0.9 resulting in lesser friction resistance on the microchannel walls. Consequently, the value of Po  
 279 drops indicating the smallest amount of pressure drop in microchannels at  $F_c = 0.9$ . It can be seen that in low and high  
 280 cavity fractions, SHS with aligned square holes and posts can impose a great effect on pressure drop through  
 281 microchannel, respectively. However, the differences between Po in staggered and aligned patterns are negligible at  
 282 low cavity fraction and become more distinctive as the surface cavity increases. This phenomenon can be also

283 demonstrated by ramping up the hydraulic slip length on the SHS as the cavity fraction steps up (Fig. 8) and the fluid  
 284 flows a longer distance without experiencing wall shear stress.  
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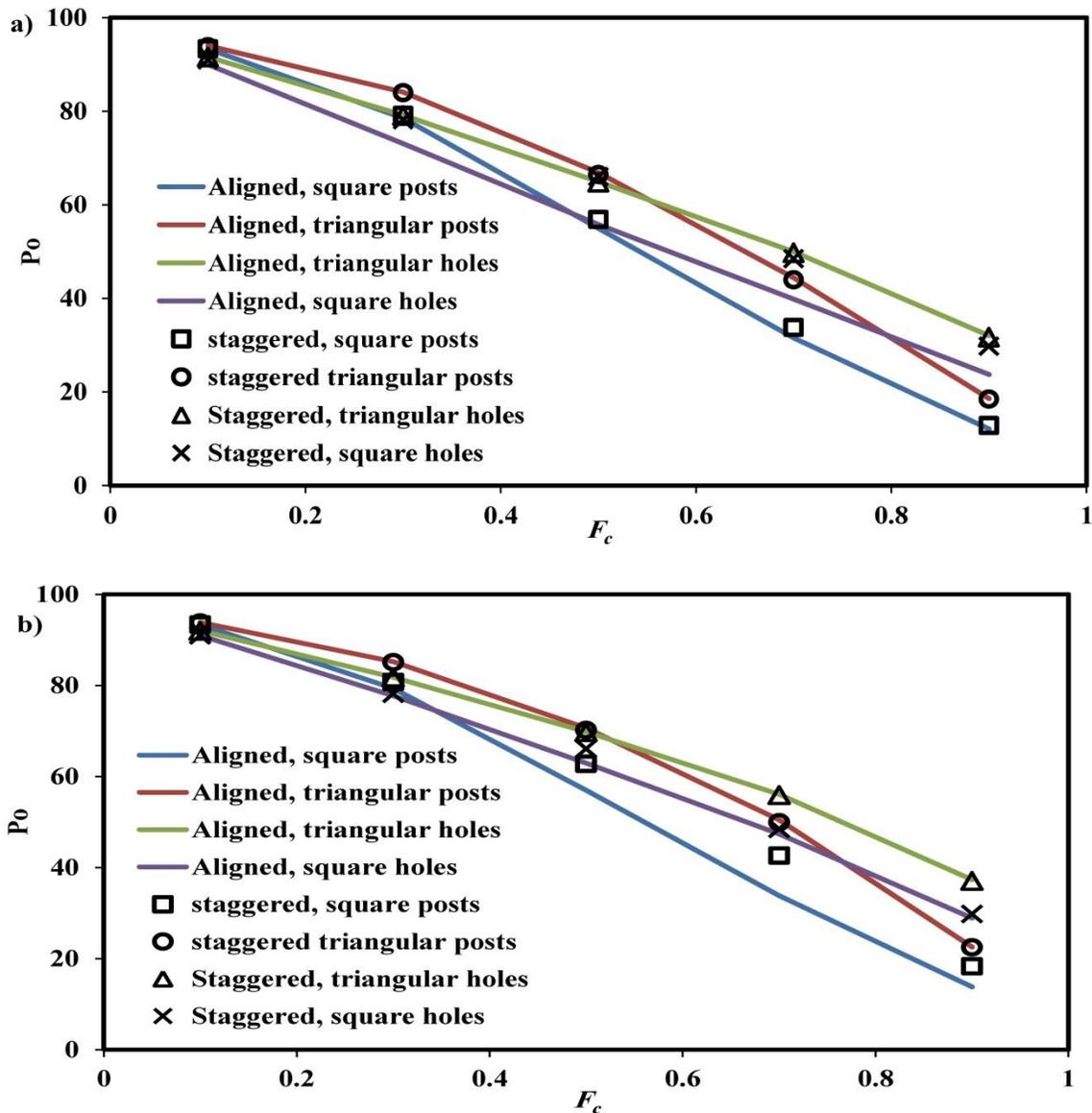


Fig. 7. Impact of cavity fraction on the Poiseuille number for different patterns at a)  $Re = 10$  b)  $Re = 100$ .

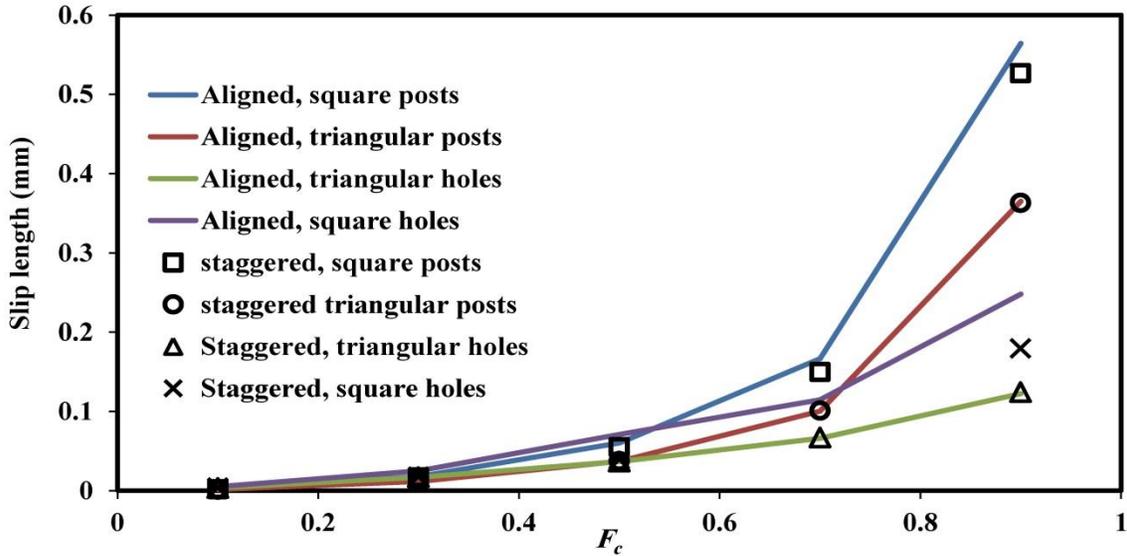
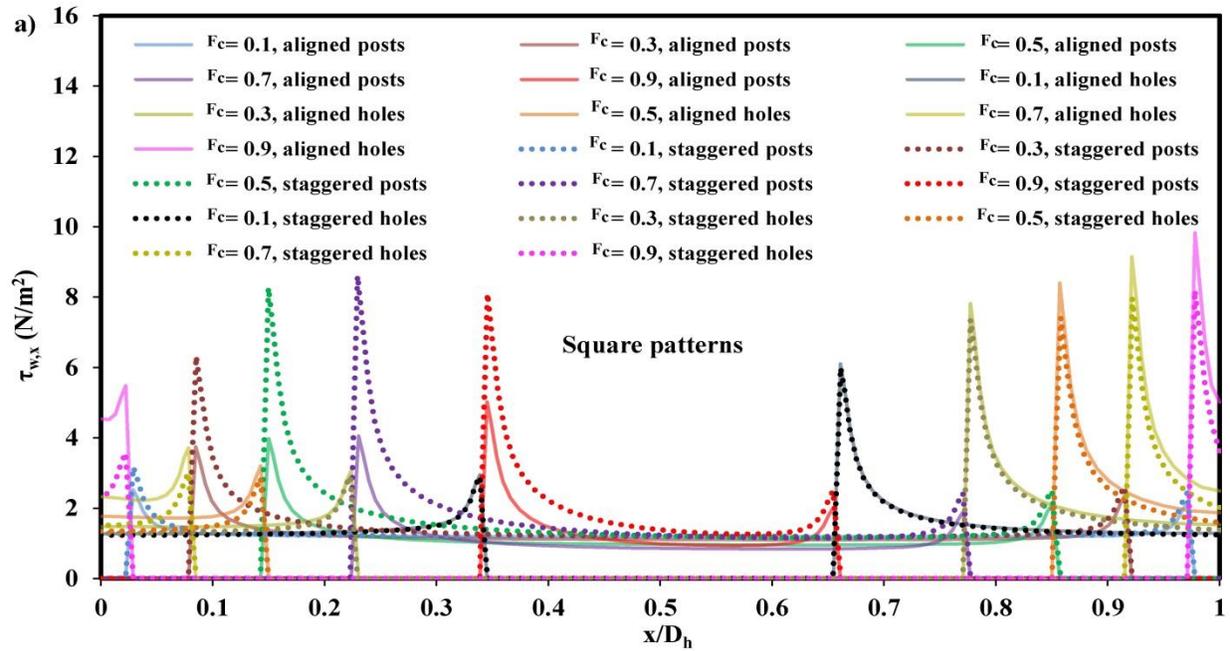
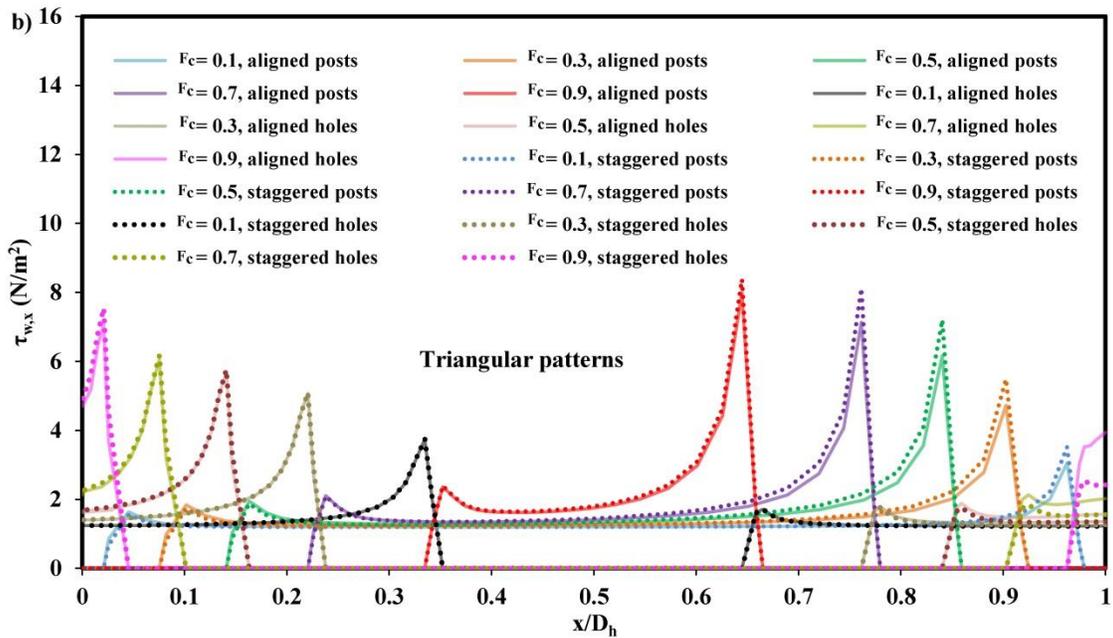


Fig. 8. The effect of cavity fraction on the slip length at  $Re = 10$ .

Although the overall wall shear stress declines by the increment of cavity fraction, the local amount of this parameter enhances as the acceleration and deceleration of particles become notable at the entering and leaving edges of the microstructures. The local distribution of wall shear stress along the flow direction is illustrated in Fig. 9 for different cavity fractions and geometries versus non-dimensionalized microchannel length for a) square and b) triangular patterns at  $Re = 100$ . As the graphs show, generally, the maximum amount of local shear stress occurs at  $F_c = 0.9$  for square micro-holes and triangular micro-post in aligned pattern. Nonetheless, the highest value of average surface shear stress on the SHS can be seen at  $F_c = 0.1$  due to the dominance of no-slip wall to cavity area. Thereupon, the Poiseuille number within the microchannel declines by the rise of cavity fraction in all cases as the slip-boundaries grow. Considering staggered microposts, fluid particles pass the longer way than aligned patterns when they depart a post to the adjacent one, which consequently leads to a higher velocity and stronger local shear stress. However, these passage lengths in the triangular patterns are almost the same and the differences in local shear stress are negligible (Fig. 12).



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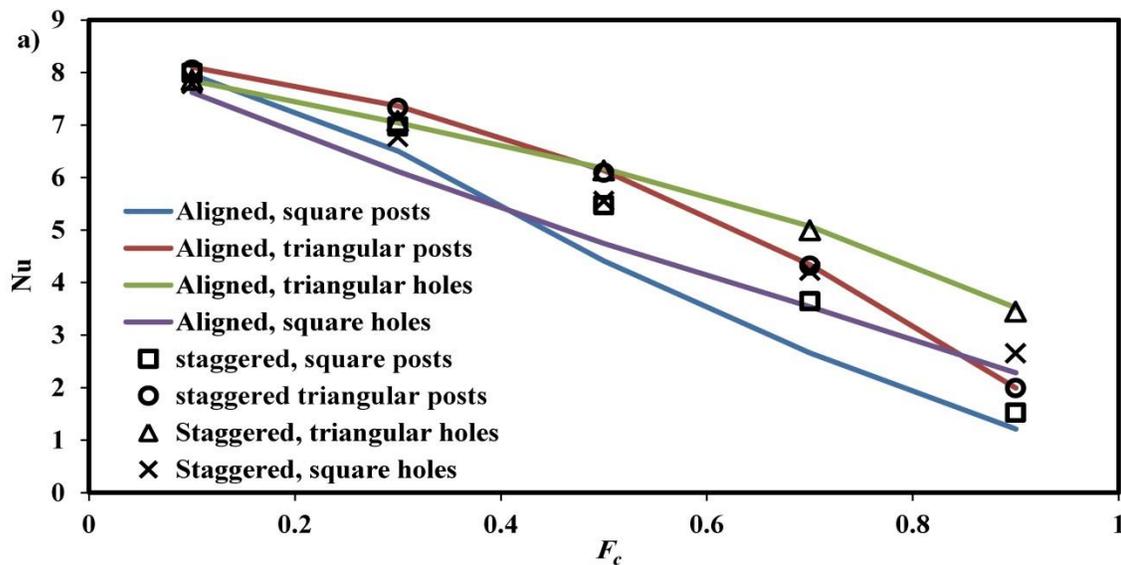
Fig. 9. Local wall shear stress versus various cavity fractions for a) square and b) triangular patterns at  $Re = 100$ . Solid lines denote aligned and dotted lines denote staggered configurations.

3.2. Heat transfer

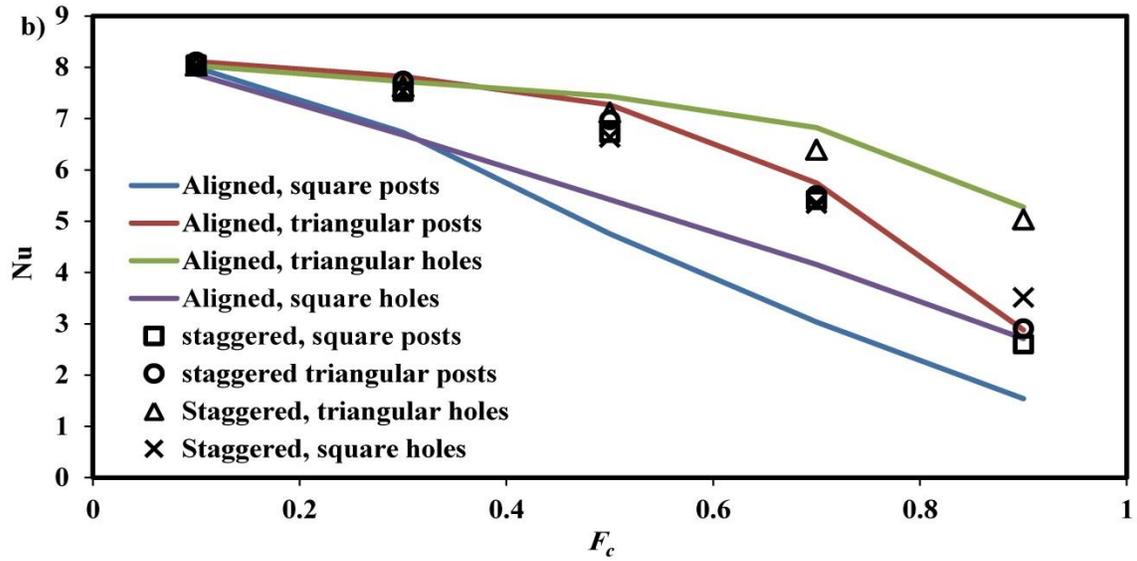
315 Nusselt number fluctuations against cavity fraction are represented for different patterns in Fig. 10a for  $Re = 10$   
 316 and Fig. 10b for  $Re = 100$ . The Nusselt number tends to reach the value of 8.235 in conventional microchannel with  
 317 constant wall heat flux at the lowest cavity fraction. It can be realized that SHS have an adverse effect on the overall  
 318 thermal performance of the microchannel. However, the local Nusselt number increases as the cavity fraction rises.  
 319 The values of local Nusselt number are demonstrated in Fig. 11 for different patterns at  $Re = 100$  and  $F_c = 0.5$ . The  
 320 results show that the minimum and maximum values of the local Nusselt number occur at the aligned square micro-  
 321 posts and micro-holes, respectively.

322 The Nusselt number also increases by the rise of Reynolds number. Fig. 12 demonstrates this impact on the  
 323 different superhydrophobic patterns. This figure indicates that the aligned triangular posts and holes pattern have the  
 324 best heat transfer performance at low and high cavity fractions for all  $Re$ . However, aligned square holes and posts  
 325 depict the worst performance at small and massive cavity fraction at all Reynolds numbers. Further, square  
 326 configurations take advantage of being staggered in terms of thermal performance while it makes negligible  
 327 differences for triangular patterns.

328 Staggered configurations bring about enhanced Nusselt number for square patterns but have a detrimental impact  
 329 on the triangular configurations. This is due to the fact that in staggered square posts, working fluid passes the long  
 330 distance before confronting the adjacent posts leading to higher velocity of particles and thinner thermal boundary  
 331 layer. Regarding square holes, displacing the microstructures results in the smaller passage of particles over the solid  
 332 surfaces and increase of thermal performance accordingly.



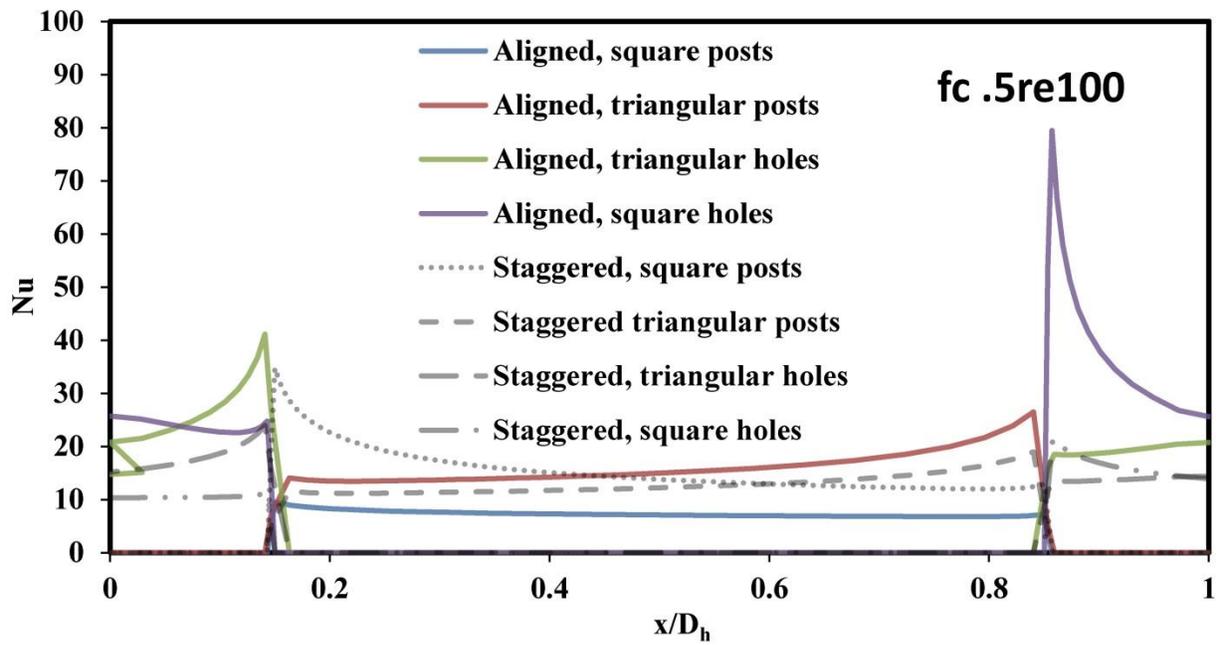
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Fig. 10. The effect of cavity fraction on the Nusselt number for different patterns at a)  $Re = 10$  b)  $Re = 100$ .



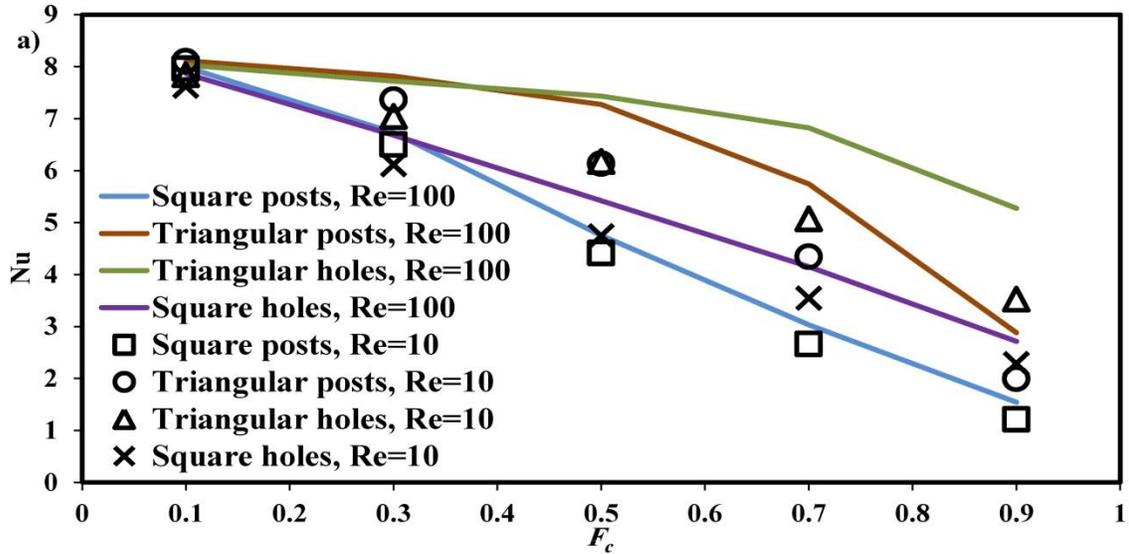
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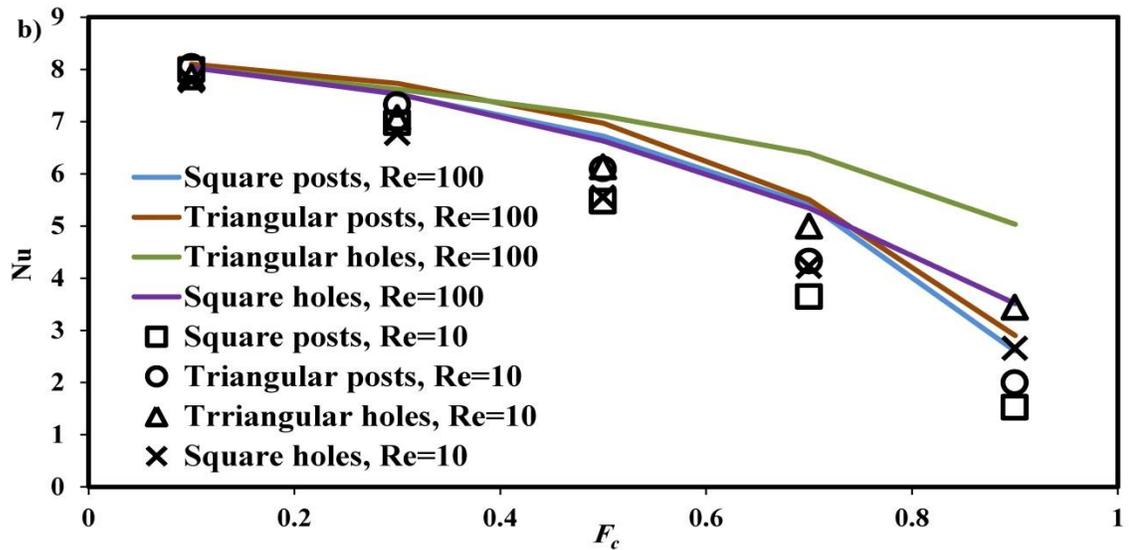
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Fig. 11. Comparison of the local Nusselt numbers for different patterns at  $Re = 100$  and  $F_c = 0.5$ .



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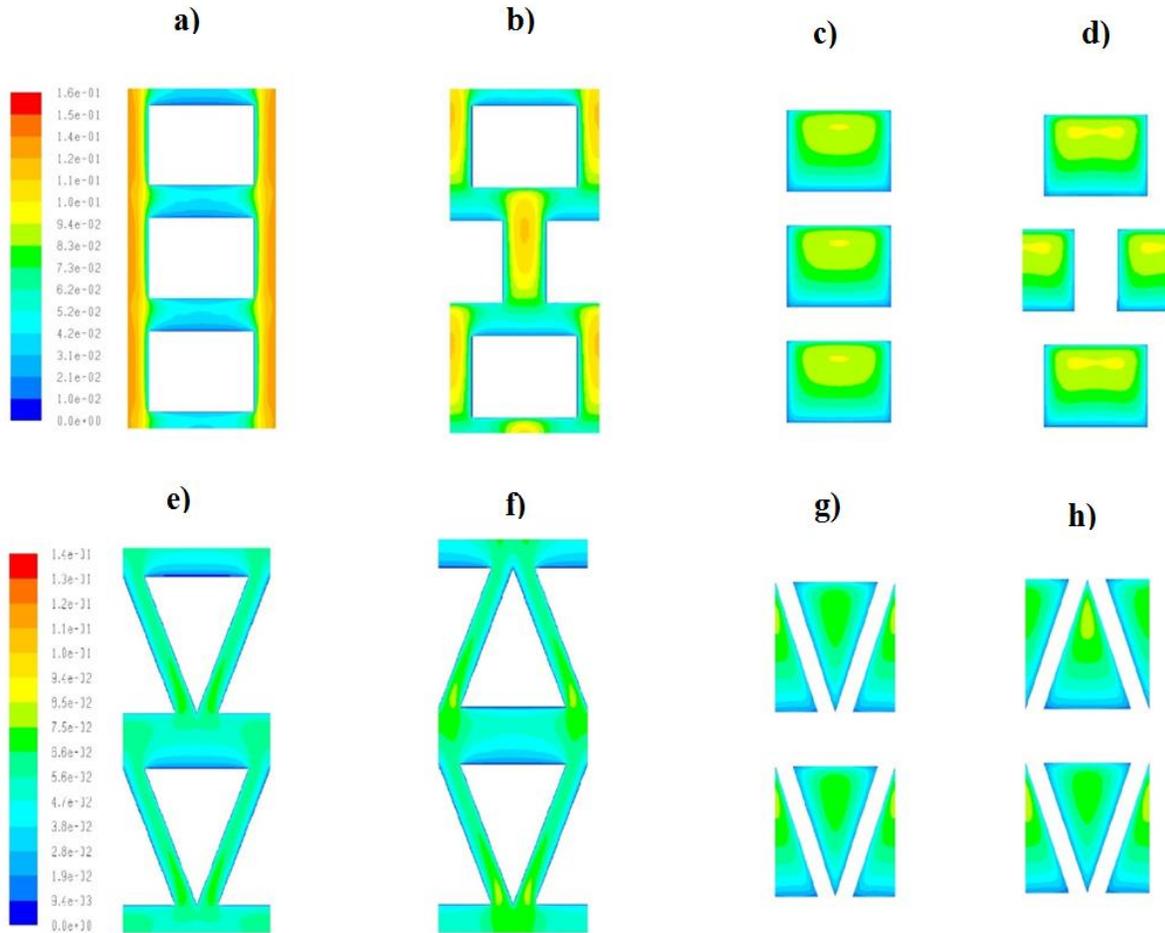
344 **Fig. 12.** Impact of Reynolds number on the Nusselt number at various cavity fractions for a) aligned and b)  
 345 staggered patterns.

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347 Fig. 13 depicts the contour of velocity magnitude over microchannel wall for diverse patterns at Reynolds number  
 348 of 100 and cavity fraction of 0.5. As can be seen in square micro-posts, a part of fluid flow is always over shear—free  
 349 interface resulting in higher pressure drop through the microchannel and lower Nusselt number. However, in staggered  
 350 configuration, heat transfer is superior due to the thinner thermal boundary layer as the fluid particles pass the long  
 351 distance over no-shear interface and speed up. Likewise, considering aligned square micro-holes, a part of fluid is  
 352 always in contact with the solid section leading to the low pressure drop, thicker thermal boundary layer and  
 353 consequently lower convective heat transfer through SHS than that of staggered configuration.

354 In sharp contrast to the situation encountered in micro-holes, the heat transfer in SHS comprising aligned  
 355 triangular micro-posts is stronger than that of staggered one. This is because the fluid particles confronting the cavity-  
 356 solid and only solid interface after leaving trailing edge of triangular micro-posts in aligned and staggered  
 357 configurations, respectively. As triangular micro-holes are concerned, fraction of the fluid flow over solid interface in  
 358 staggered patterns is more than that over the aligned configuration. This behavior leads to enhanced heat transfer in  
 359 aligned triangular micro-holes.

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364 **Fig. 13.** Velocity magnitude contour at  $Re = 100$  and  $F_c = 0.5$  for a) aligned and b) staggered square micro-posts,  
 365 and c) aligned d) staggered square micro-holes as well as e) aligned and f) staggered triangular micro-posts, and g)  
 366 aligned and h) staggered triangular micro-holes. The solid (no-slip) surfaces are illustrated in white color.

367

### 368 3.3. Overall thermal performance of SHS

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Although SHSs can curtail the pressure drop through microchannels, they also lead to lower [heat transfer rate in comparison to that over conventional surfaces of microchannels](#). This means that the effect of SHSs should be

371 considered simultaneously when it comes to the applications and significance of SHS in thermal issues. Therefore, a  
372 microchannel with the maximum heat transfer and minimum pressure drop is desirable.

373 For comparison between thermal and hydrodynamic aspects of SHS, goodness factor can be defined as [56]:

$$\varphi = \frac{NuPr^{-1/3}}{fRe}, \quad (10)$$

374  
375 in which, Prandtl number is represented by  $Pr$ . This parameter is constant for a fully developed laminar flow with a  
376 specific wall heat flux within parallel plate and equal to

$$\varphi_c = \frac{8.235 \times 7.56^{-1/3}}{96}. \quad (11)$$

377  
378 Considering this value as a reference, a thermal performance index can be defined as the ratio of  $\varphi/\varphi_c$  for overall  
379 thermal assessment of SHS, expressed by [57]:

$$\eta = \frac{\varphi}{\varphi_c} = \frac{(Nu/fRe)}{(8.235/96)}. \quad (12)$$

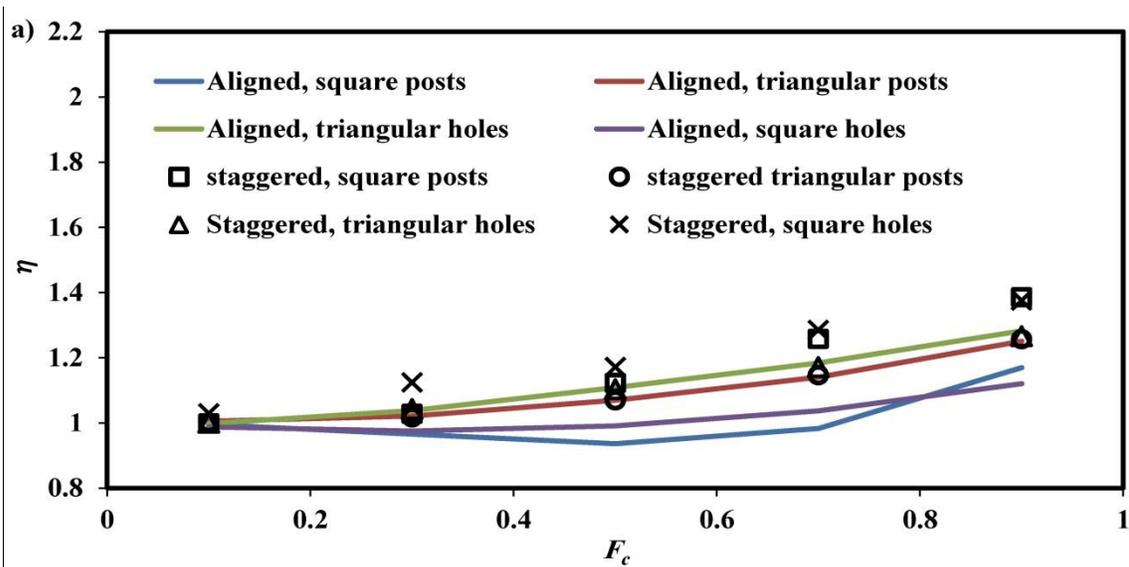
380  
381 This index is compared and shown for alternative microstructures and Reynolds numbers at different cavity  
382 fraction in Fig. 14. The upgraded thermal performance can be seen when  $\varphi/\varphi_c > 1$  in comparison with the  
383 conventional microchannel at the same pumping energy utilization [47]. The interesting point is that the thermal  
384 performance indices of triangular configurations are always higher than unity indicating the preeminence of this SHS  
385 over a smooth microchannel. Generally, this parameter increases by the rise of Reynolds number and cavity fraction  
386 for all geometries. Also, the increment of Reynolds number leads to the higher value of the index for all investigated  
387 cases. However, the smooth microchannels are more advantageous than square structures at small values of  $Re$  and  $F_c$   
388 as the values of thermal indices become less than unity.

389 The staggered square micro-hole shows its superiority at lower Reynolds numbers while the staggered square  
390 posts tend to have a better overall performance at larger  $Re$ . Although staggered square hole and posts demonstrate  
391 the highest values of goodness factor at low  $Re$ , they are aligned triangular hole and staggered square posts that  
392 represent the best performance at higher  $Re$ . The smallest overall performance is devoted to the aligned square holes  
393 and posts. The  $\eta$  graphs imply that the lowest ratio of goodness factor belongs to the aligned square micro-holes and  
394 micro-posts, although the chief impact of displacing the microstructures from aligned to staggered applies to these  
395 two patterns.

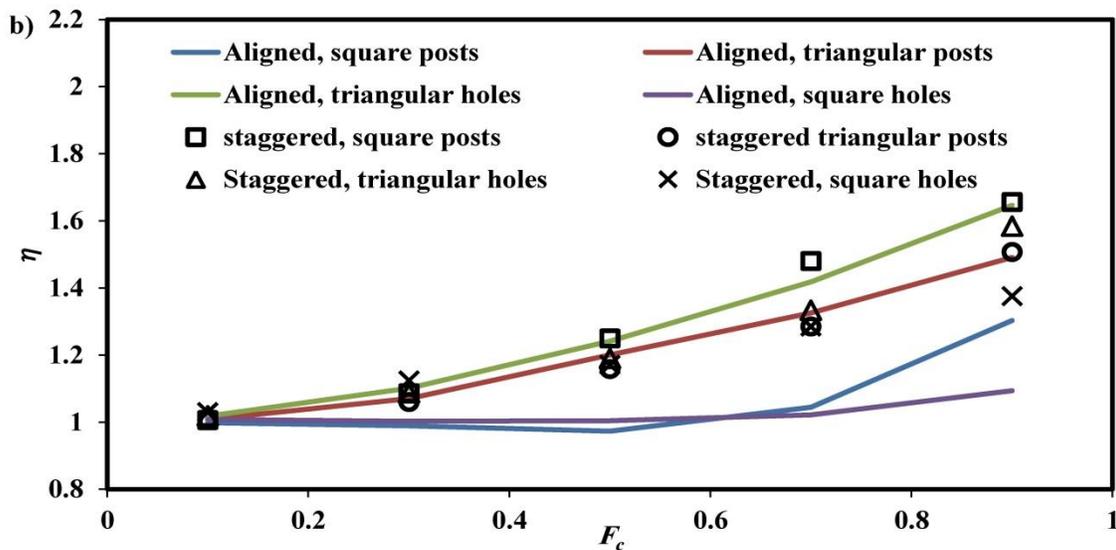
396 In most cases with triangular geometries, displacing microstructures makes considerable differences except at  
397 higher  $Re$  and  $F_c = 0.9$ . Nonetheless, as the heat transfer at low Reynolds number is weak, generally, higher values  
398 of  $Re$  are applied for cooling purposes. Overall, the rise of cavity fraction triggers the lower values of Nusselt number  
399 but a higher value of thermal index. This is since the reduction rate of pressure through the microchannel is more

400 significant than that of heat transfer through walls, in other words, the effect of shear-free interface on drag reduction  
 401 is more dominant than the decrement of heat transfer resulting in higher overall thermal performance of SHSs.

402 The use of goodness factor provides a rigorous way of optimizing the design. In case of using these patterned  
 403 microchannels, the application and circumstances are of great importance. This means that if the drag reduction is of  
 404 more importance than thermal performance of SHS, then the microchannel with aligned square micro-posts is an ideal  
 405 selection requiring the lowest power for pumping the fluid through the microchannel. Yet, triangular holes as well as  
 406 staggered square holes are ideal for enhancing heat transfer at low and high Reynolds numbers, respectively. Further,  
 407 staggered square holes and posts are the top choices considering overall performance of the patterned microchannels.  
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 412 **Fig. 14.** Impacts of cavity fraction on thermal performance index for different patterns at a)  $Re = 10$  b)  $Re = 100$ .

413 **4. Conclusions**

414 The use of SHSs with triangular microstructures for enhancing the performance of microchannels has so far  
415 received limited attention. To address this issue, microchannels with superhydrophobic surfaces consisting of square  
416 and triangular micro-posts and micro-holes were investigated numerically in a fully developed laminar flow. The  
417 impacts of cavity fractions, Reynolds numbers and various patterns were examined through evaluating the overall  
418 thermal performance, Poiseuille and Nusselt number of the microchannel. The key outcomes of this study are  
419 summarized in the followings.

- 420 • The rise of cavity fraction leads to the decline of the required pumping power and Nusselt numbers. Yet, the  
421 thermal performance index, as the simultaneous indicator of hydraulic and thermal performances, increases.
- 422 • At low Reynolds numbers and cavity fractions, the effect of SHSs is negligible and the system tends to behave  
423 like a conventional microchannel with smooth walls. However, the significant influences of SHS can be  
424 clearly seen at higher  $Re$  and  $F_c$ .
- 425 • By escalation of cavity fraction, total shear stress and heat transfer over the microchannel wall diminish while  
426 the local values surge.
- 427 • Triangular micro-posts and -holes configurations have the maximum heat transfer rates at the low and high  
428 cavity fractions for all  $Re$  respectively.
- 429 • The largest goodness factor ratio is attainable at high values of Reynolds number and cavity fraction,  
430 specifically, with patterns of staggered square holes and post at low and high values of Reynolds number.
- 431 • Triangular patterns have the best heat transfer performance. Triangular microstructures can be beneficial for  
432 all Reynolds numbers and cavity fractions when the total performance of microchannel is concerned. This is  
433 because the effect of shear-free interface on drag reduction is more dominant than the decrement of heat  
434 transfer for triangular patterns.

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